

Powder Blending in the PAT Era

Current Research and Resources



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Outline of Presentation

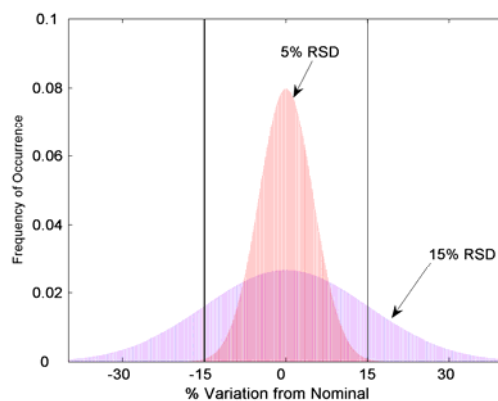
- Basics of Powder Blending
- Critical Parameters Affecting Performance
- Effect of Blending on Product Quality
- (Optical) PAT Sensors for Monitoring & Analysis
 - Case Study: Blend Analysis via NIR Imaging Spectroscopy
 - Case Study: Efficient Calibration
 - Case Study: Advanced Endpoint Criteria
- Future Directions in Pharma Blending

Basics of Powder Blending

- Objective: Mechanical agitation of powder mixtures to achieve uniformity
- Mixture Classifications:
 - Ordered
 - ♦ Interaction between major and minor component
 - ♦ Size mis-match between components
 - ♦ Uniformity is independent of sample scale
 - ♦ Cohesive particles
 - Partially-ordered
 - Random
 - ♦ Equal size/weight particles
 - ♦ Little or no surface interaction ($>100\ \mu\text{m}$)
 - ♦ Level of uniformity is dependent on sample scale

Basics of Powder Blending

- Measurement of Blend Uniformity:
 - Between-Sample Variance (σ^2)
 - Maximizing Uniformity \approx Minimizing Variance (at a given scale)



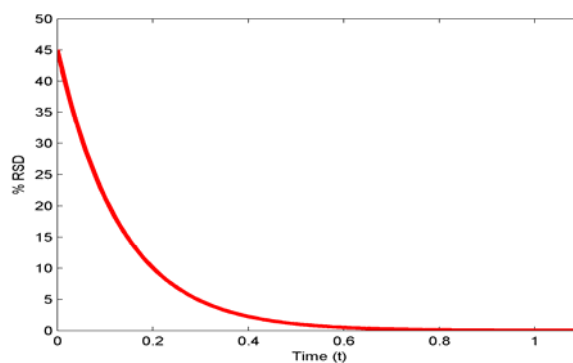
Basics of Powder Blending

- Mixing Mechanisms:
 - Diffusion
 - ♦ Random particle movement throughout powder bed
 - ♦ Dominant mechanism for tumbling powder blenders (e.g. bin-, V-blenders)
 - Convection
 - ♦ *En masse* movement of large volumes within powder bed
 - ♦ Dominant mechanism for stationary mixers with moving parts (e.g. Hobart mixer, ribbon blender, etc.)
 - Shear
 - ♦ Mixing occurs along slip planes between regions of particles
 - ♦ Often considered a combination of diffusion & convection
 - ♦ Level of shear is controlled by rate of kinetic energy transfer to particles (e.g. intensifier bar)

Basics of Powder Blending

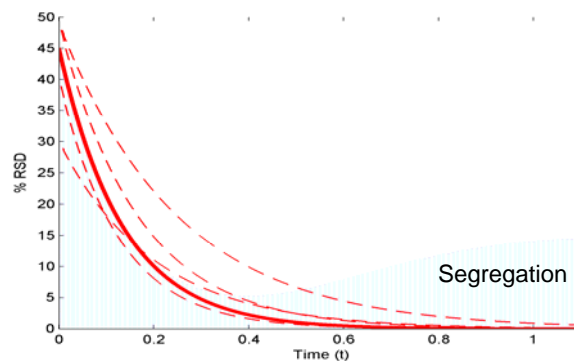
- Mixing Rate: $\sigma_t^2 = Ae^{-(k_{diff} + k_{conv} + k_{shear})wt}$

- w = rate of rotation, agitation
- t = time
- k = rate constant for mixing
- A = arbitrary constant



Basics of Powder Blending

- **Mixing Rate:** $\sigma_t^2 = Ae^{-\sum k_{unk,t,c,h} wt} + P_{seg,t,w,c}$
 - Most pharmaceutical powder blends are **seperable**, with **stochastic rate**
 - Finite probability of spontaneous segregation (“de-mixing”)
 - True (observed) rate is a function of many **uncontrolled** variables



Critical Parameters Affecting Performance

- **Particle Morphology Distribution**
 - **Size**
 - ♦ Often cited as most critical variable
 - ♦ Smaller particles “sift” while larger particles “float”
 - ♦ Size mismatch can be detrimental or beneficial, depending on mechanism and classification of mixing
 - **Shape**
 - ♦ Impacts rate of particle interaction, cohesiveness
 - **Density**
 - ♦ Larger, more dense particles will have greater momentum
- **Cohesiveness**
 - More cohesive powders have limited ability to flow
 - Tendency to aggregate with other cohesive particles, induces size segregation
 - Cohesive powder beds are more likely to create motionless “voids”
- **Friability**

Critical Parameters Affecting Performance

- Mixer design
 - Mechanism of mixing most affected by design
 - Symmetry tends to reduce blending efficiency
- Rotational speed
 - Increases energy intensity and the rate of diffusion and/or convection
 - Large, dense particles can be entrained by centrifugal force
- Fill level
 - Excessive fill level decreases blend efficiency, increases likelihood of voids
- Loading configuration
 - Minor components can become “trapped”
- Energy Intensity (e.g. intensifier speed)
 - Reduces incidence of agglomerates
 - Can cause excessive attrition, change in crystallinity




Critical Parameters Affecting Performance

- Ambient conditions
 - Variation in humidity will significantly affect the ability of the particles to dissipate charge
- Mixture composition
 - Un-controlled variation in concentration of components (assay) or quality of individual constituents will interact with other factors

Effect of Blending on Product Quality

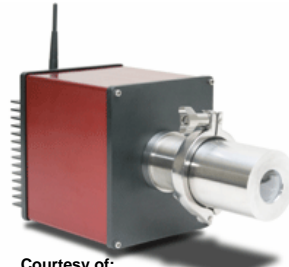
- Critical quality attributes (CQAs) form the basis for PAT risk assessment
 - Priority of PAT sensors and controls should be defined by impact on risk to CQAs
- CQAs affected by blending performance:
 - Content Uniformity
 - Assay (loss of material)
 - Physical uniformity
 - ◆ Micro-distribution/interaction of powders
 - ◆ Crystallinity, compactibility, etc.

Objectives of PAT in Blending

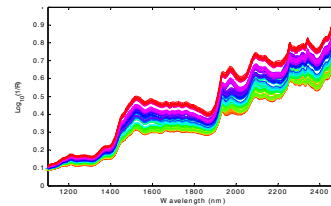
- Blending is often the key critical control point
 - Directly effects multiple CQAs
 - Blend performance is a complex, multivariate function:
 - ◆ Most factors have multiple interactions
 - ◆ Many factors have limited or no controls
- Objectives of PAT for blending:
 1. Minimize risks to product quality
 - ◆ Critical quality attributes (CQAs)
 2. Maximize production efficiency
 - ◆ Reduction of cycle time (C/T)
 3. Facilitate process understanding

PAT Sensors for Monitoring and Analysis

- NIR Spectroscopy
 - Basics:
 - ♦ Measurement of absorbance via diffuse reflectance
 - ♦ (Relatively) deep sample penetration
 - ♦ Spectra are sensitive to chemical and **physical** quality of mixture
 - Method development
 - ♦ Qualitative (peak monitoring, etc.)
 - ♦ Quantitative
 - Current methods can be onerous
 - Commercial Viability/Background
 - ♦ In-line NIR research has been public for >10 years
 - ♦ Multiple (relatively) low-cost instrumentation choices
 - ♦ RF Wireless sensors available OTC
 - ♦ Deployment will soon be “algorithmic”



Courtesy of:
Control Developments, Inc.

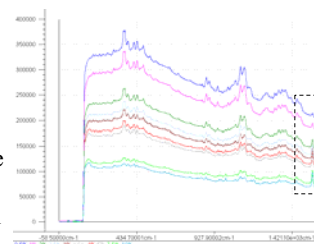


PAT Sensors for Monitoring and Analysis

- Raman Spectroscopy
 - Basics:
 - ♦ Measurement of inelastic scatter intensity
 - ♦ Shallow sample penetration
 - ♦ Spectra are more less sensitive to excipients
 - ♦ Mostly robust to physical sample interactions
 - Method development
 - ♦ Specificity for API is usually more direct
 - Commercial Viability/Background
 - ♦ Raman blend monitoring research is more recent, builds upon NIR experience
 - ♦ Choice of in-line instrumentation is much more limited
 - ♦ Wireless Raman spectrometers are not yet available



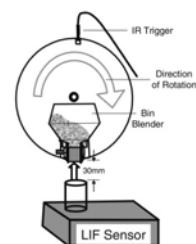
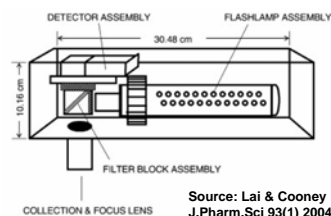
Source: Arwa El Hagrasy
ASQ Fall Tech, 2004



PAT Sensors for Monitoring and Analysis

• Laser-Induced Fluorescence

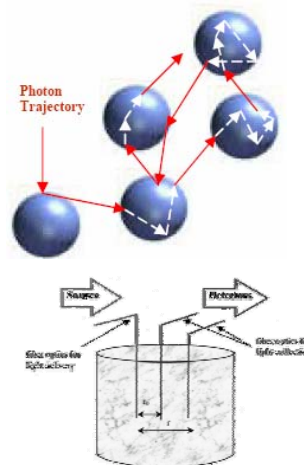
- Basics:
 - ♦ Measurement of short-lifetime fluorescence induced by high-energy pulse from flashlamp
 - ♦ Shallow sample penetration
 - ♦ Choice of flashlamp and detector filters determine sensitivity
- Method development
 - ♦ Complete specificity
 - ♦ Low sensitivity to excipients (uses background signal)
- Commercial Viability/Background
 - ♦ Continues to be prototypical?



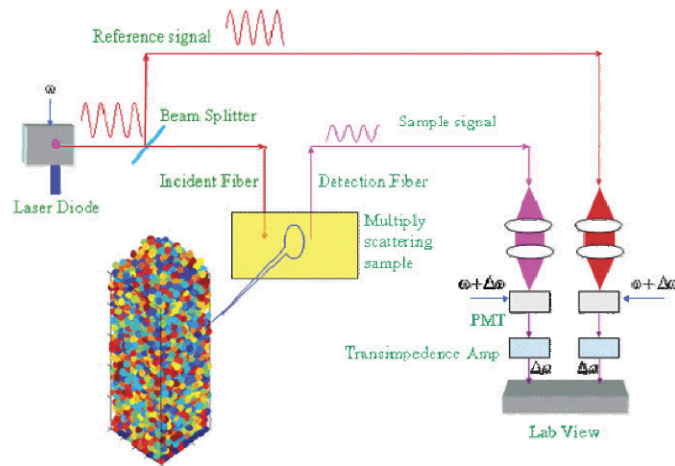
PAT Sensors for Monitoring and Analysis

• Frequency-Domain Photon Migration (FDPM)

- Basics:
 - ♦ Measurement of the change in frequency and phase of radiation during in-sample diffusion
 - ♦ Can independently measure particle size and optical absorbance
 - ♦ effectively separates scatter and absorption
- Method development
 - ♦ Materials constants must be known for prediction & calibration
 - Refractive index
 - Powder bed solid fraction
- Commercial Viability/Background
 - ♦ Fully prototypical
 - ♦ May be an ideal extension of NIR



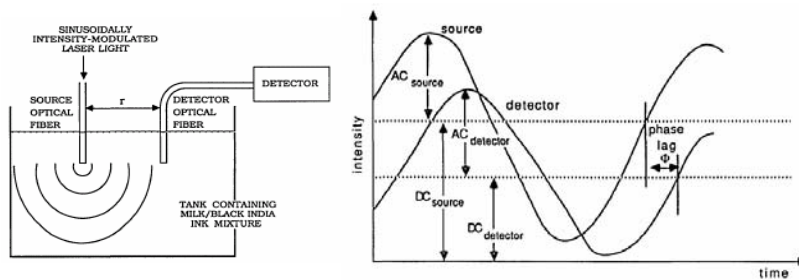
Frequency-Domain Photon Migration (FDPM)



Pan T.S., Sevick-Muraca E.M. J. Pharm. Sci. 2006, 95:530-541

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Frequency-Domain Photon Migration (FDPM)



- Light-density wave is measured in term of relative AC, DC and PS:
 - AC: the amplitude of the light intensity oscillation
 - DC: average light intensity
 - PS: phase shift

Fishkin J.B. and Gratton E. J. Opt. Soc. Am. A. 1993,10: 127-140

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PAT Sensors for Monitoring and Analysis

- NIR Imaging Spectroscopy
 - Basics:
 - ♦ Measurement of microscopic/ macroscopic distribution of diffuse reflectance
 - ♦ Image resolution limited by depth of penetration/ diffusion
 - Method development
 - ♦ Requires two levels:
 - calibration+image analysis
 - ♦ Single-image calibration is often feasible (using curve resolution, etc.)
 - ♦ Currently, blend homogeneity is assessed using histogram description statistics
 - Commercial Viability/Background
 - ♦ At-line instruments available OTC
 - ♦ In-line instrumentation is in prototypical development

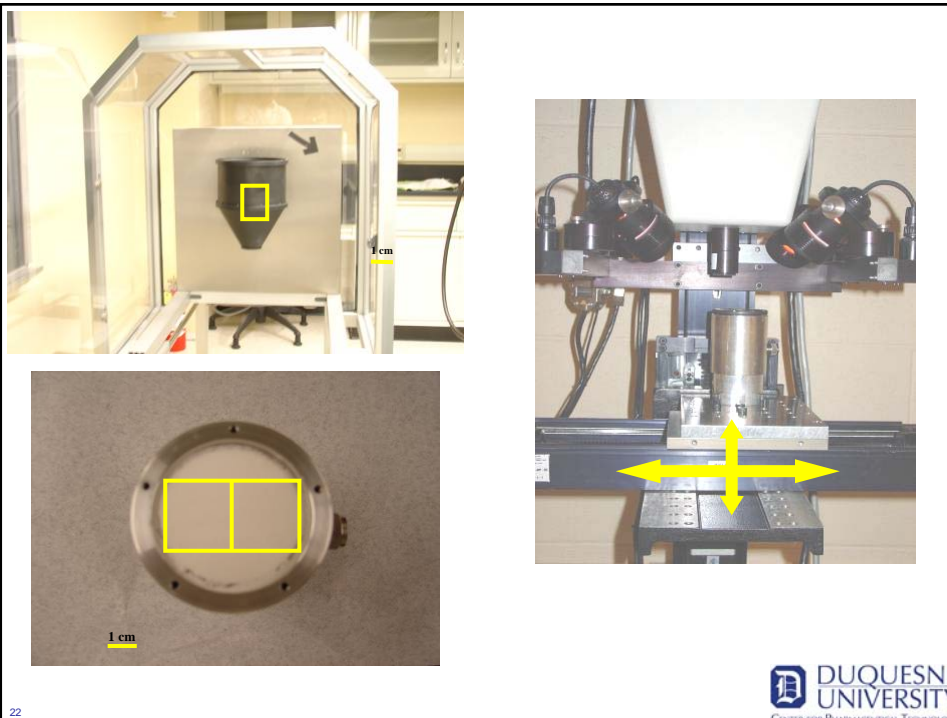


Case Study: NIR Imaging Spectroscopy

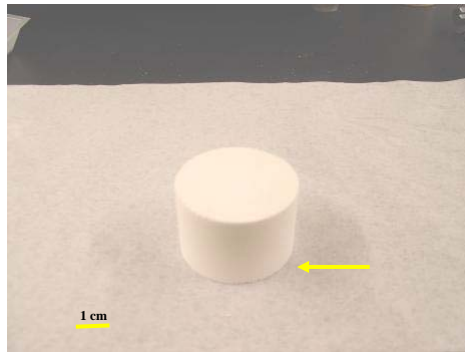
- Dissertation work of [Hua Ma](#) at Duquesne
 - For questions/comments: mah@duq.edu
- Objectives:
 - Establish imaging as an effective tool for characterization of blending
 - ♦ **End Point** - correlation between imaging method and traditional monitoring methods
 - ♦ **Critical Blending Areas** – optimal sampling locations
 - ♦ **Distribution of Components** (API & Excipients) – distribution variability during blending

Case Study: NIR Imaging Spectroscopy

- **Materials:**
 - APAP (powder, 150 μ m, 5%)
 - MCC (PH 200, 180 μ m, 31.7%)
 - Lactose (Fast-Flo[®] monohydrate, 100 μ m, 63.3%)
- **Imaging and UV Sampling Time Points:**
 - 10 identical three component mixtures (30g/mixture) corresponding to 10 time points:
0.5, 1, 2, 5, 10, 15, 20, 25, 30, 40 minutes (10 time points)
- **Equipment:**
 - Aluminum mini blender
 - MatrixNIR[™] imaging system
 - ♦ FOV: 17.2 \times 21.5 mm (0.5X objective)
 - ♦ Wavelength Range: 1400-1675nm, 5 nm interval
 - HP 8543 UV-Vis spectrometer
- **Bin charging order:** Lactose, MCC, APAP



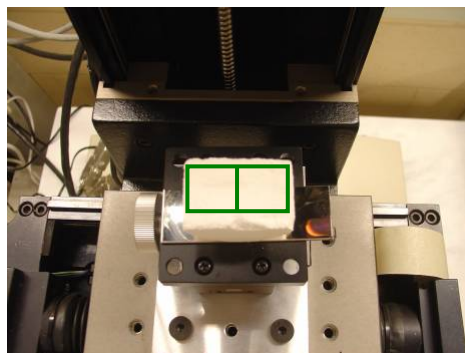
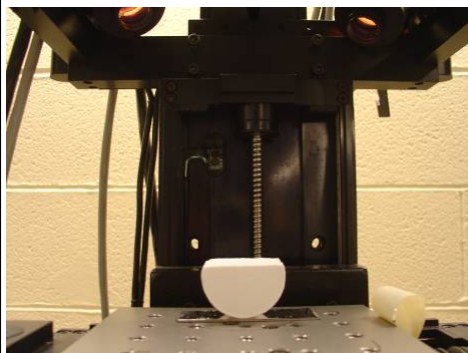
Case Study: NIR Imaging Spectroscopy

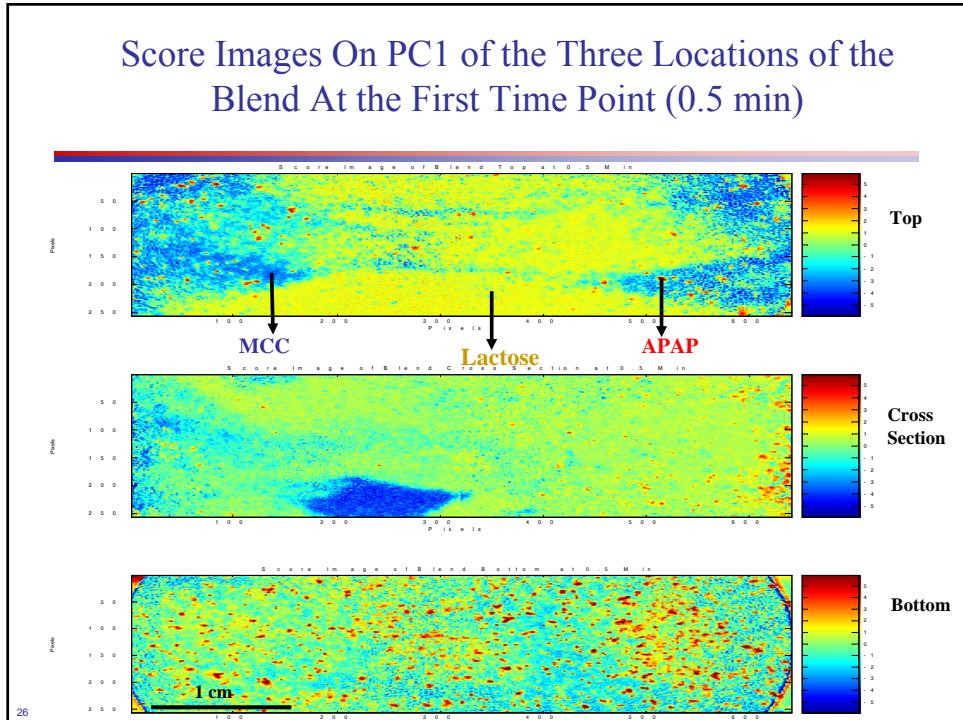
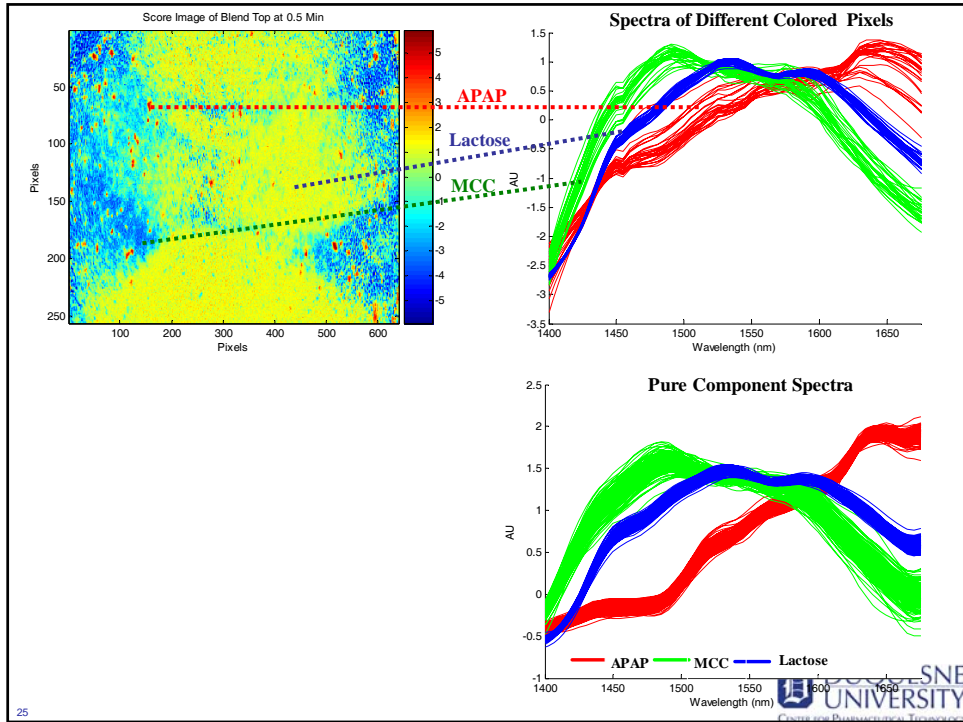


Compression Force: 1200 Pounds

Dwell Time: 30 Seconds.

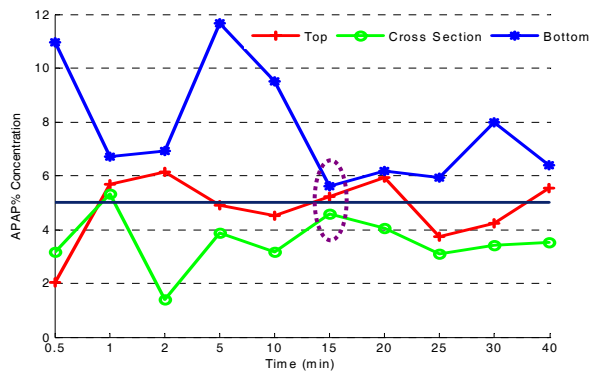
Case Study: NIR Imaging Spectroscopy





Case Study: NIR Imaging Spectroscopy

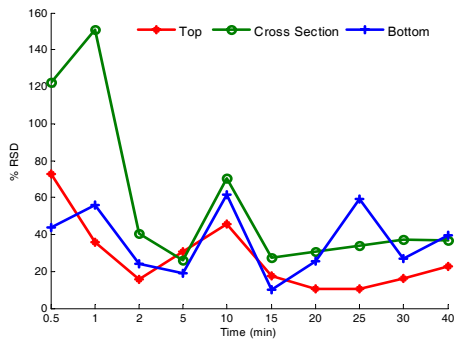
Overall Predicted APAP Concentration at Three Locations



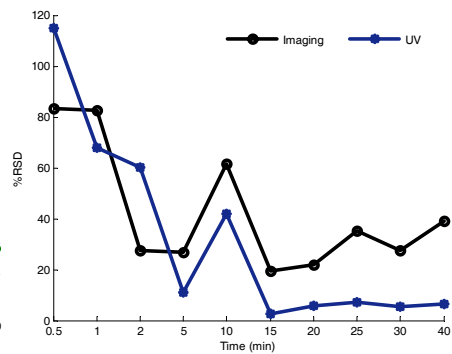
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Case Study: NIR Imaging Spectroscopy

%RSD Change in Three Locations of the Blend

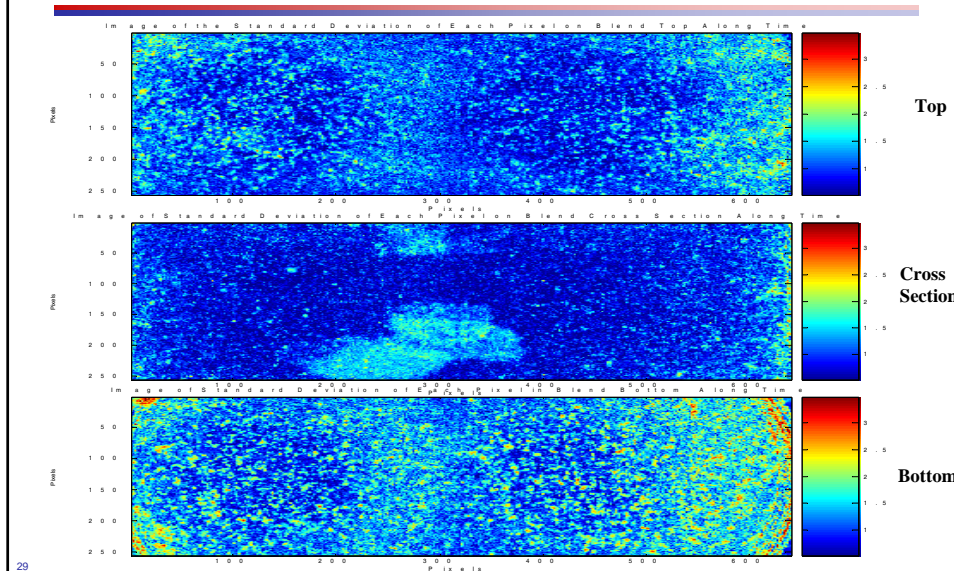


Correlation %RSD Profiles Between UV and Imaging Analysis



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Temporal Spectral Variation Map



Case Study: NIR Imaging Spectroscopy

- Conclusions
 - Imaging spectroscopy was successful in providing a rapid estimate of the distribution of chemical components
 - Imaging spectroscopy identified key understanding of the (model) process:
 - ◆ A dead zone exists in the current configuration; may be related to cohesiveness of materials or fill level
 - ◆ Substantial differences in the rate of mixing was observed for different portions of the mixer
 - ◆ Correlation with (traditional) UV-VIS sampling was observed

Case Study: Efficient Method Development

- Quantitative analysis is more powerful
 - Directionality is important for root cause analysis
 - Easier to determine limits
 - Results can be scaled according to risk
- Empirical calibration is expensive
 - Development of high-leverage training samples
 - Reference chemistry/lab time
- Calibration should be (relatively) simple
 - Number of components known
 - Interference effects are expected (hardness, particle size, density, etc.)
 - Pure-component spectra are generally available
 - Concentrations vary over a very narrow range
 - ◆ Linearly additive

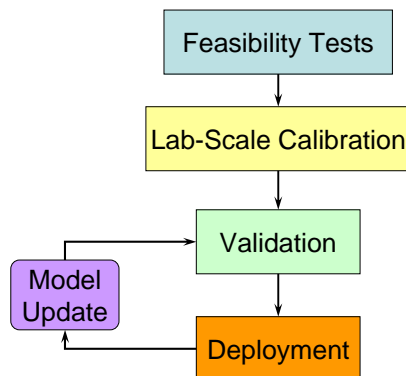
With everything we know, why must (calibration) be so costly?



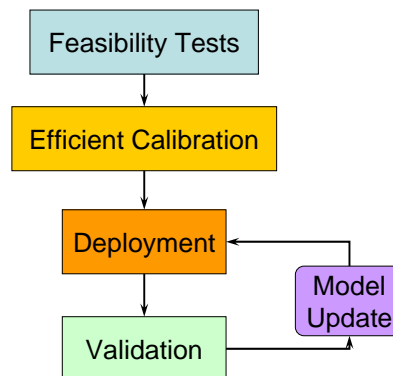
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Case Study: Efficient Method Development

**Current Method
Development Path:**

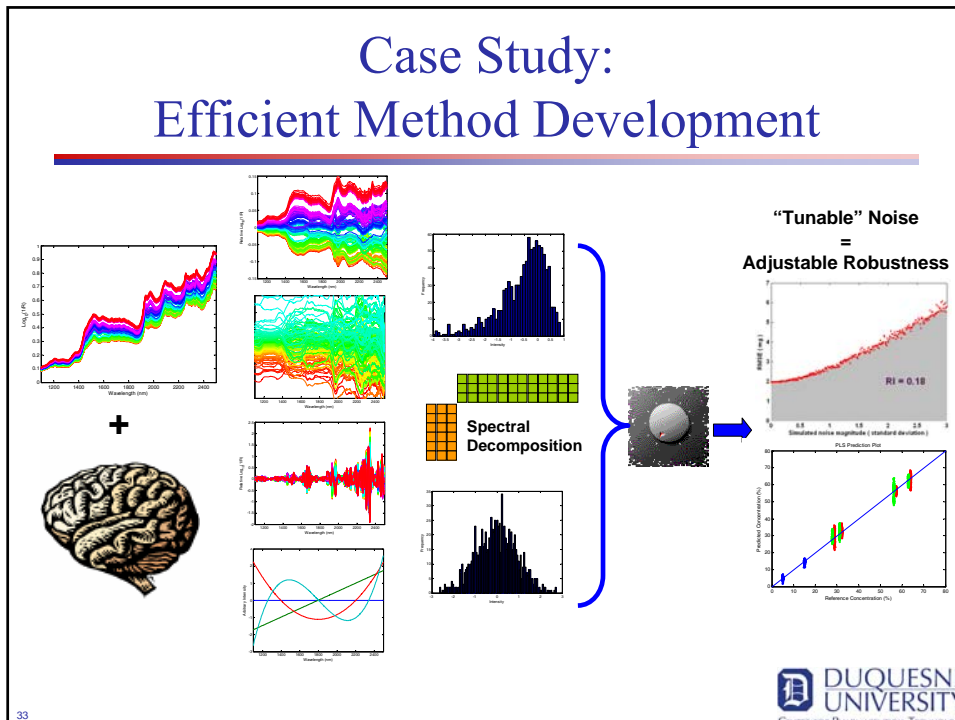


**Efficient Calibration
Development Path:**



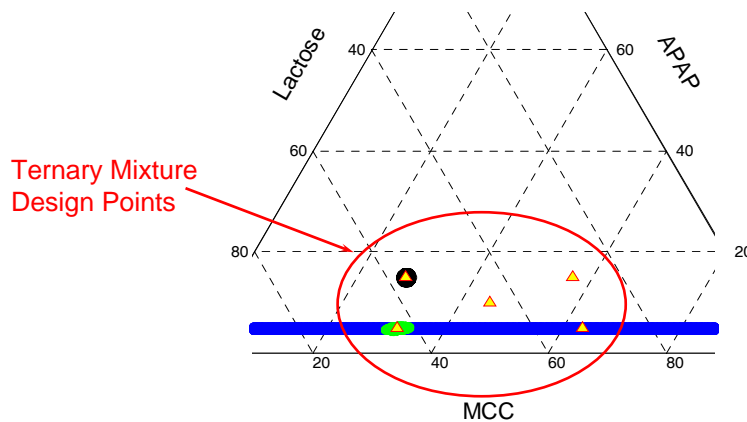
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Case Study: Efficient Method Development



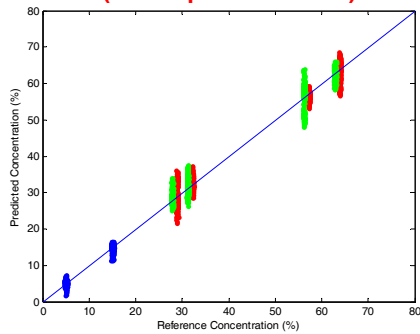
Case Study: Efficient Method Development

- Trial Blending DOE Study



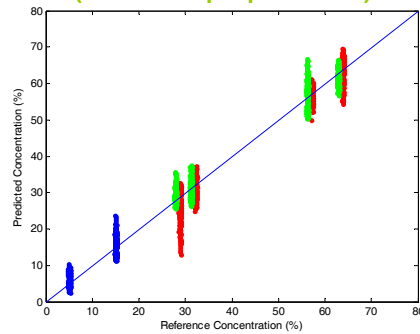
Case Study: Efficient Method Development

**PLS Calibration
(in-sample estimation)**



$R^2 = 0.991$
SEC = 2.0

**Synthetic Calibration
(out-of-sample prediction)**



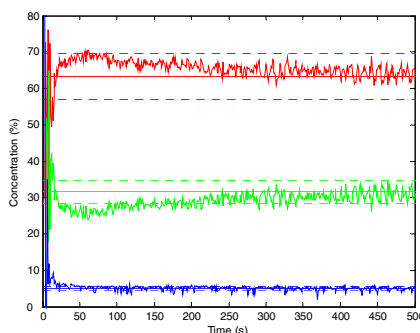
$R^2 = 0.976$
SEP = 3.2



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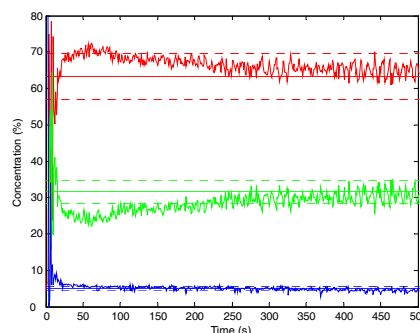
Case Study: Efficient Method Development

**PLS Calibration
(in-sample prediction)**



$R^2 = 0.991$
SEC = 2.0

**Synthetic Calibration
(out-of-sample prediction)**



$R^2 = 0.976$
SEP = 3.2



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Case Study: Efficient Method Development

- Synthetic calibration should be considered as an extension of current efforts in efficient calibration
 - PCP, maximum-likelihood weighting, direct orthogonalization
- Conclusions:
 - Synthetic calibration was observed to yield a calibration model having **sufficiently-suitable** performance using **zero** high-leverage samples or reference chemistry

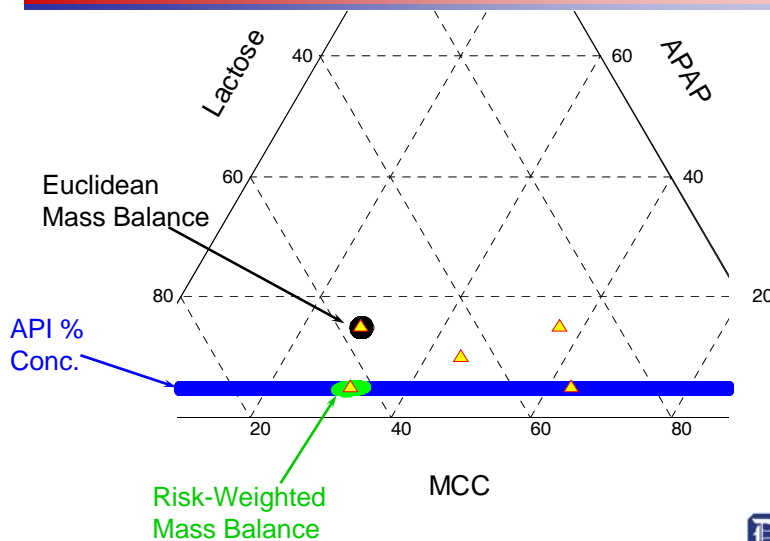
Case Study: Advanced Endpoint Criteria

- Current endpoint criteria for PAT monitoring of blending are mainly an adaptation of traditional criteria
 - RSD of API must be less than 5%
 - Does not consider absolute concentration of API, concentration of excipients, or distribution of excipients
 - Individual components of mixture will often have unique mixing rate constants
- In a PAT-enabled environment, **additional information** should be leveraged to **improve control**
 - Balance of constituents (e.g. lactose/MCC) is important to minimizing variation in tablet quality
 - ♦ Physical characteristics
 - ♦ Dosage form performance (disintegration, release)
 - Better control of blending will mitigate the risk of poor quality through tableting, and will reduce the need for feedback control of tablet press
 - Acceptance limits (μ , σ) should be reflective of relative risk to CTQs posed by variance in the individual component

Case Study: Advanced Endpoint Criteria

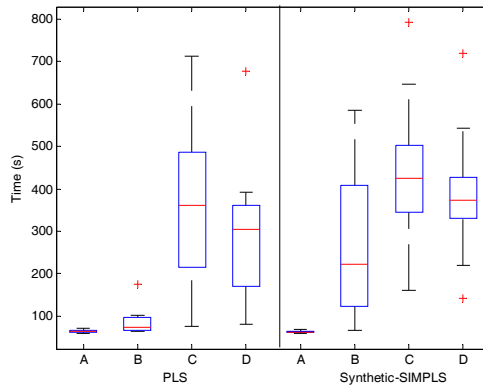
- Endpoint criteria examined during comparative research studies at DCPT:
 - API variance: moving-window student's t-test of RSD
 - API concentration: moving-window t-test of API concentration
 - Equal-weighted mass-balance: equal-weighted moving-window t-test of RMS deviation from nominal (planned) concentration
 - Risk-weighted mass-balance: weighting on importance of individual components in determining endpoint is adjusted according to risk to CTQs
 - ◆ Will often be more "lenient" than equal weighting
 - ◆ Risk weighting can be determined by observed variance patterns (e.g. mahalanobis distance) or based on **design space**
 - ◆ Risk weighting can be "fine-tuned" as the level of process understanding increases

Case Study: Advanced Endpoint Criteria



Case Study: Advanced Endpoint Criteria

- Key:
 - A = API % RSD
 - B = API Conc. t-test
 - C = Equal-Wt. Mass Balance
 - D = Risk-Weighted Mass-Bal
- Y-Axis:
 - Distribution of identified endpoints (n = 24) for each criterion

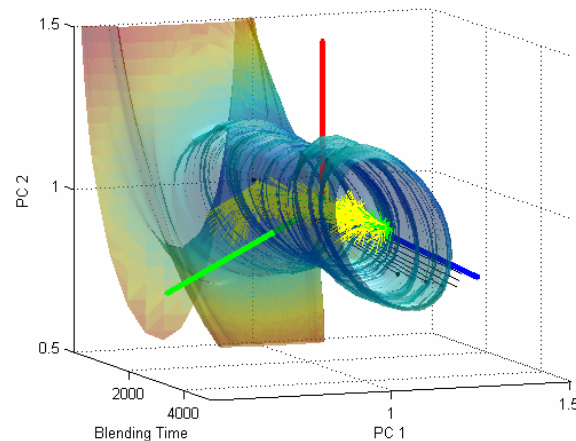


Case Study: Advanced Endpoint Criteria

- Conclusions
 - Traditional, API variance endpoint criterion consistently underestimated the time required to reach homogeneity in all constituents
 - ◆ May be a “lurking effect” since release tests may not directly assess these conditions
 - Risk-weighted (mahalanobis) criterion tended to reach the endpoint sooner, and with less variance in endpoint, than the equal-weighted strategy
 - As level of understanding is increased (e.g. correlation between blend uniformity/composition and F.G. quality), the size of acceptance region can be adjusted to update the new reality for the design space

The Future of Blending

- Higher levels of process understanding:



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The Future of Blending

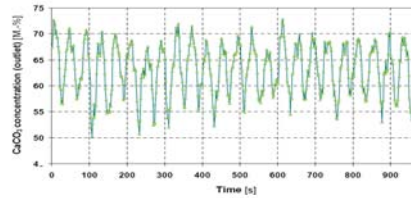
- Feed-forward/ feed-back process control models
 - How will blending data be integrated with control and real-time-release models?
 - ◆ Level 1: Binary (yes / no) (current state)
 - ◆ Level 2: Descriptive (N = 14 rotations, RSD = 1.4%)
 - ◆ Level 3: Component-specific rate constants, statistics
 - ◆ Level 4: Whole trajectory modeling? Use in predicting instantaneous CpK thru tableting? (desired state?)

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The Future of Blending

- Continuous Processing:

- Current technologies:
 - ♦ Horizontal tumbling (Munson)
 - ♦ Continuous fluid-bed
 - ♦ “motionless mixers”
- Much work has already been done...(in other industries)
- Real-time analytics and controls will be key



Kehlenbeck & Sommer
2002 World Congress on Particle Technology

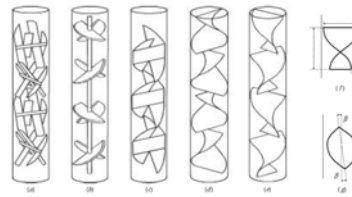


Fig. 1 Examples for motionless mixers also applicable for bulk solids.
(a) horizontal double (HDS) mixer, (b) flow (FDS) mixer, (c) Kenics mixer, (d) Kenics static mixer, (e) P&M mixer, (f) or-taper and (g) P&M elements of a P&M mixer

J. Gyenis, Kona 2002



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Parting Shots:

- The evolution of philosophies on pharmaceutical powder blending:
 - Old:
 - “(PK says) it takes 30 minutes...call me when its finished...”
 - New:
 - “Is it done yet? Why is there so much variability?”
 - Future:
 - “Based on up-stream measurements, this blend will be done in ~14 rotations...see you at compression”



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Acknowledgements:

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- Dr. Carl A. Anderson
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- Hua Ma (May)
- Zhenqi Shiz (Pete)
- Steven Short
- Spectral Dimensions (now Malvern)
- Control Developments, Inc.



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